# STUDIES ON SEPARATION OF IRON OXIDE AND FLOTATION OF SILICA FROM KASHMIR BAUXITE

BY P. K. DESHPANDE AND G. N. BHAT

(Department of Chemical Technology and Chemical Engineering, Indian Institute of Science, Bangalore-3)

Received July 12, 1954

Different bauxite consuming industries generally demand bauxites of varying specifications.<sup>1</sup> Aluminium and chemical industries desire to have the iron oxide content in the raw material bauxite less than 6 and 2 per cent. respectively. This paper presents results of flotation experiments designed to separate iron oxide and silica from bauxite.

#### MATERIALS, METHODS AND RESULTS

The sample of bauxite and methods of analysis are the same as used in the previous investigation.<sup>2</sup> Effects of aniline, T.T. mixture (o-toluidine + Thiocarbanilide 1:1) and sodium hexametaphosphate as depressants for iron oxides under different pH conditions were studied and the results are represented graphically in Figs. 1, 2 and 3.



FIG. 1. Effect of Aniline and T.T. Mixt. on the Depression of Fc<sub>2</sub>O<sub>3</sub>



FIG. 2. Effect of pH on the Depression of Fe<sub>2</sub>O<sub>3</sub>

.

FIG. 3. Depression of Fe<sub>2</sub>O<sub>3</sub> by Sodium Hexametaphosphate

# Studies on Separation of Iron Oxide from Kashmir Bauxite 55

Bauxite samples were roasted for half-an-hour in a reducing atmosphere in a furnace in order to favour the reduction of hematite in the ore to magnetite. The roasted mass was dropped in cold water, dried and subjected to dry magnetic separation in a Sterns laboratory magnetic separator. Roasting at different temperatures were studied and the overall results are given in Table I.

TABLE 1										
Fractions	2 1.22 12	Wt. %	Ignition loss %	SiO <sub>2</sub> %	Fe <sub>3</sub> O <sub>1</sub> %	TiO₂ %	Al <sub>2</sub> O <sub>3</sub> %	Separation of iron oxide %		
				Temperati	ure 450° C.		-			
Concentrate Tailings Composite	••	20 80 100	3 · 12 8 · 10 7 · 10	12.81 11.71 11.93	34 · 13 4 · 12 10 · 12	4 · 30 3 · 21 3 · 42	45 · 64 72 · 86 67 · 62	67 · 45		
				Temperat	ure 550° C.					
Concentrate Tailings Composite	•••	15 85 100	3 · 50 7 · 90 7 · 24	12 · 40 11 · 80 11 · 89	25 · 94 6 · 01 9 · 00	4 · 50 3 · 22 3 · 41	53 · 66 71 · 06 68 · 46	43.24		
	-			Temperat	ure 650° C.					
Concentrate	• •	30	5.41	12.21	16-91	3.91	61.56	50.26		
Tailings		70	7.85	11.78	7.18	3.21	69.98			
Composite	••	100	7.12	11.91	10.10	3.42	67.45			
			, <u>,,,,,,,,,,,,,,,,</u> ,,,,,,,,,,,,,,,,,,,	Temperat	ure 750° C.					
Concentrate	1. NO.	35	5.86	12.06	14-05	3.75	64.28	48 · 50		
Tailings	• /•	65	7.82	11.83	8.02	3.22	69.11			
Composite		100	7.14	11.92	10.14	3.42	67.38			

Experiments were also carried out to depress silica from the original one in the first instance and subsequently depress iron oxide from the concentrate so obtained. Results are given in Table II.

					the second se	
Reagents used	Ignition loss %	SiO <sub>2</sub> %	Fe <sub>2</sub> O <sub>3</sub>	TiO <sub>2</sub> %	Al <sub>2</sub> O <sub>3</sub> %	% Al <sub>2</sub> O <sub>3</sub> recovery
Original ore	14.15	11.81	7.90	3-41	62.73	
Oleic acid, Pine oil, Kerosene, Sod. silicate Aniline, Pine oil T.T. mixture, Pine oil	14 · 73 14 · 78 14 · 77	6 · 88 6 · 89 6 · 88	7 · 93 4 · 98 4 · 41	3 · 14 3 · 14 3 · 15	67 · 32 70 · 21 70 · 79	65 · 19 65 · 19 64 · 79
Sod. hexametaphos- phate, Pine oil Oleic acid, Pine oil,	14.81	6.86	5 · 33	3-14	69.86	63 • 96
Sod. hexametaphos- phate	14.84	<b>6 · 7</b> 1	5.44	3.12	69·89	81.96
	Reagents used Original ore Oleic acid, Pine oil, Kerosene, Sod. silicate Aniline, Pine oil T.T. mixture, Pine oil Sod. hexametaphos- phate, Pine oil Oleic acid, Pine oil, Kerosene, Sod. silicate, Sod. hexametaphos- phate	Reagents usedIgnition loss %Original ore14.15Oleic acid, Pine oil, Kerosene, Sod. silicate14.73Aniline, Pine oil14.78T.T. mixture, Pine oil14.77Sod. hexametaphos- phate, Pine oil14.81Oleic acid, Pine oil14.81Oleic acid, Pine oil, Kerosene, Sod. silicate, Sod. hexametaphos- phate14.84	Reagents usedIgnition loss %SiO2 $\%$ Original ore14.1511.81Oleic acid, Pine oil, Kerosene, Sod. silicate14.736.88Aniline, Pine oil14.786.89T.T. mixture, Pine oil14.776.88Sod. hexametaphos- phate, Pine oil14.816.86Oleic acid, Pine oil, Kerosene, Sod. silicate, Sod. hexametaphos- phate14.846.71	Reagents usedIgnition loss %SiO2 % $Fe_2O_3$ %Original ore $14 \cdot 15$ $11 \cdot 81$ $7 \cdot 90$ Oleic acid, Pine oil, Kerosene, Sod. silicate $14 \cdot 73$ $6 \cdot 88$ $7 \cdot 93$ Aniline, Pine oil $14 \cdot 73$ $6 \cdot 88$ $7 \cdot 93$ Aniline, Pine oil $14 \cdot 78$ $6 \cdot 89$ $4 \cdot 98$ T.T. mixture, Pine oil $14 \cdot 77$ $6 \cdot 88$ $4 \cdot 41$ Sod. hexametaphos- phate, Pine oil $14 \cdot 81$ $6 \cdot 86$ $5 \cdot 33$ Oleic acid, Pine oil, Kerosene, Sod. silicate, Sod. hexametaphos- phate $14 \cdot 84$ $6 \cdot 71$ $5 \cdot 44$	Reagents usedIgnition loss $\frac{N}{6}$ SiO2 $\frac{N}{6}$ Fe2O3 $\frac{N}{6}$ TiO2 $\frac{N}{6}$ Original ore14.1511.817.903.41Oleic acid, Pine oil, Kerosene, Sod. silicate14.736.887.933.14Aniline, Pine oil14.786.894.983.14T.T. mixture, Pine oil14.776.884.413.15Sod. hexametaphos- phate, Pine oil14.816.865.333.14Oleic acid, Pine oil, Kerosene, Sod. silicate, Sod. hexametaphos- phate14.846.715.443.12	Reagents usedIgnition loss %SiO2 % $Fe_2O_3$ %TiO2 % $Al_2O_3$ %Original ore $14 \cdot 15$ $11 \cdot 81$ $7 \cdot 90$ $3 \cdot 41$ $62 \cdot 73$ Oleic acid, Pine oil, Kerosene, Sod. silicate $14 \cdot 73$ $6 \cdot 88$ $7 \cdot 93$ $3 \cdot 14$ $67 \cdot 32$ Aniline, Pine oil. $14 \cdot 78$ $6 \cdot 89$ $4 \cdot 98$ $3 \cdot 14$ $70 \cdot 21$ T.T. mixture, Pine oil. $14 \cdot 77$ $6 \cdot 88$ $4 \cdot 41$ $3 \cdot 15$ $70 \cdot 79$ Sod. hexametaphos- phate, Pine oil. $14 \cdot 81$ $6 \cdot 86$ $5 \cdot 33$ $3 \cdot 14$ $69 \cdot 86$ Oleic acid, Pine oil, Kerosene, Sod. silicate, Sod. hexametaphos- phate. $14 \cdot 84$ $6 \cdot 71$ $5 \cdot 44$ $3 \cdot 12$ $69 \cdot 89$

TABLE II

[Concentrate 'B' was floated in (C), (D) and (E)]

P. K. DESHPANDE AND G. N. BHAT









FIG. 6. Effect of pH on the Composition

Influence of Rosamine D Acetate (Herculus Powder Co., Washington) and of 'Tallow Amine Acetate" (Armour & Co., Chicago) as cationic collectors on the flotation of negatively charged silica in bauxite was a'so studied at different pH conditions. The results are given in Figs. 4, 5 and 6.

## DISCUSSION

Fatty acids used in the flotation of alumina would also act as collectors for iron oxide<sup>3</sup> with consequent flotation of alumina and iron oxide together. Aniline and T.T. mixture worked effectively in depressing iron oxide (Fig. 1), but these reagents did not depress silica. Both the depressants were effective in acidic circuits only, with optimum results at pH 6.0 (Fig. 2). When sodium hexametaphosphate was, however, used in conjunction with oleic acid and sodium silicate, it depressed iron oxide efficiently without affecting the depression of silica by sodium silicate (Fig. 3).

More efficient removal of iron oxide was obtained by magnetic separation than by flotation. Lower roasting temperature seemed to favour better iron oxide separation. Such may be the case due to the reduction of hematite being favoured by lower temperature (Table 1).

Two-stage flotation yielded a better grade of concentrate but the overall alumina recovery in the final concentrate was only 65 per cent. On the other hand, the recovery noticed during single stage flotation using oleic acid, sodium silicate and sodium hexametaphosphate was of the order of 82 per cent., the grade of the product being equally satisfactory (Table II).

### P. K. DESHPANDE AND G. N. BHAT

The action of the two amines on the flotation of silica seems to be nearly the same (Fig. 4). This may be due to the fact that almost all the amines give maximum contact angles of the order of  $60^{\circ}$  as found by Wark and Wark.<sup>1</sup> Floatability of silica was found to increase with increasing pH (Figs. 5 and 6). Talmud and Lubman<sup>5</sup> have also observed that SiO<sub>2</sub> floats more readily in alkaline circuits. But, it was noticed that when low percentage of silica assay in the sink (concentrate) was obtained, alumina recovery in the sink was also low and the iron oxide assay varied from 6.67 per cent. to 7.81 per cent. Thus, better grade of sink with respect to silica and iron oxide and maximum alumina recovery could not be obtained at the same time.

#### ACKNOWLEDGEMENT

The authors wish to thank Dr. S. S. Ghosh and Dr. M. R. A. Rao for their assistance and suggestions during these investigations.

#### REFERENCES

- 1. U.S. Bur. Mines, Report Invest. R. I. 4440, (Apr. 1949).
- 2. Deshpande and Bhat ... J. Ind. Inst. Sci., 1954. 36, No. 4, 267-76.
- 3. Yudenich, G. I. and Bogdanova, Z. S. Gornyi Zhur 1952, 126, No. 10, 29-33.
- 4. Wark and Wark ... J. Phys. Chem., 1935, 39, 1029.
- 5. Talmud, D. and Lubman, N. M. ... Kolloid Zeitschrift, 1930, 50, 159-62.